

The background of the slide features a vibrant landscape. In the foreground, there is a lush green field of crops, possibly corn. Beyond the field, a calm blue body of water stretches across the middle ground. The sky above is a deep blue, filled with soft, white clouds. A large, semi-transparent rainbow arches across the entire scene, from the left side of the frame to the right, partially overlapping the text.

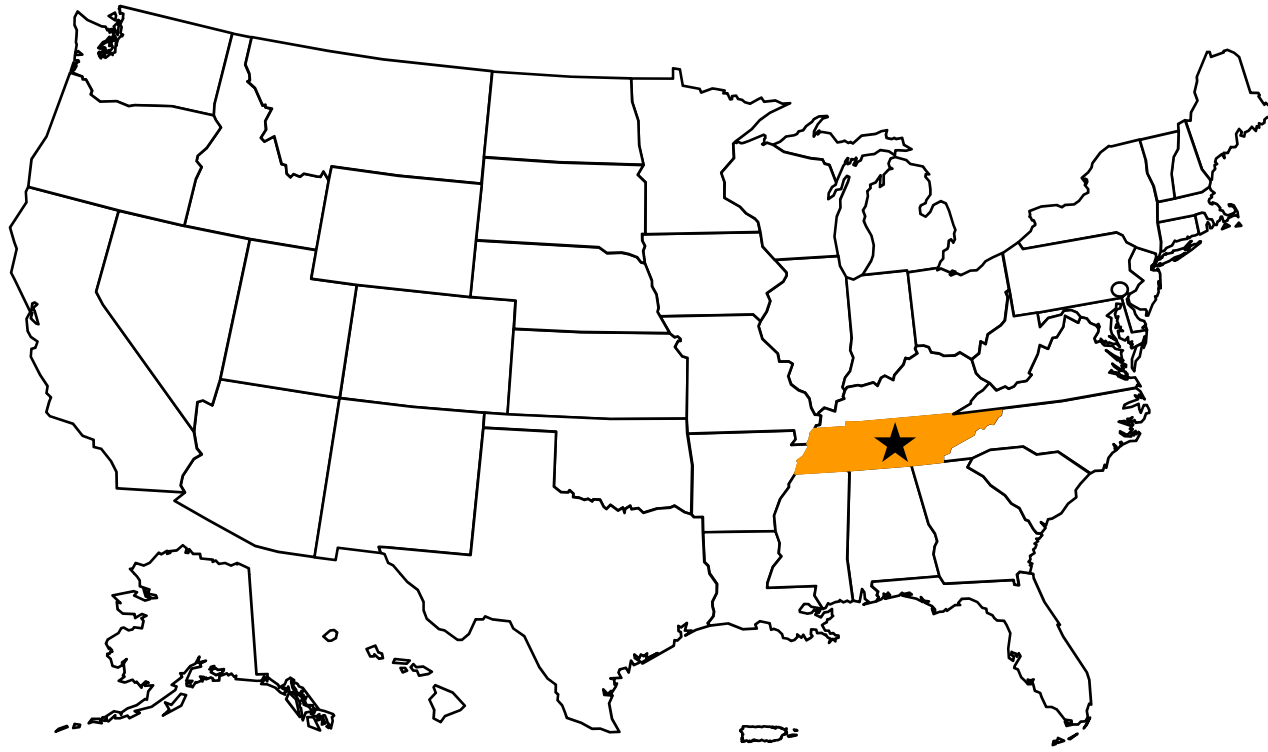
Maximizing Effluent Dispersion and Minimizing Mixing Zones

**Water Environment Federation
People to People
Beijing, China**

November 2008

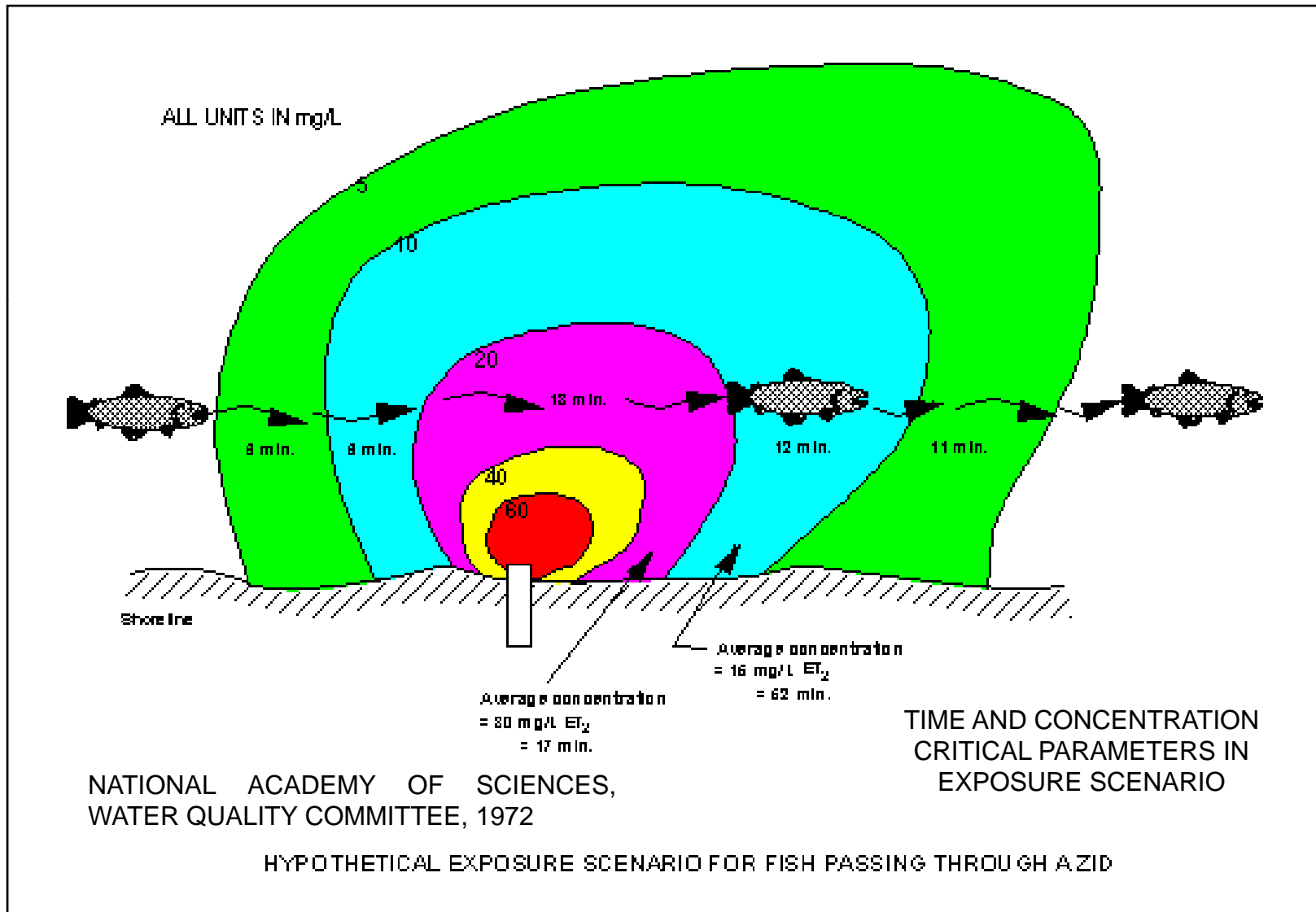
Presented by
Michael R. Corn, P.E.
President, **AquAeTer, Inc.**
Brentwood, Tennessee
USA





Grand Ole Opry
Home of Country Music

Why Do We Need Mixing Zones?



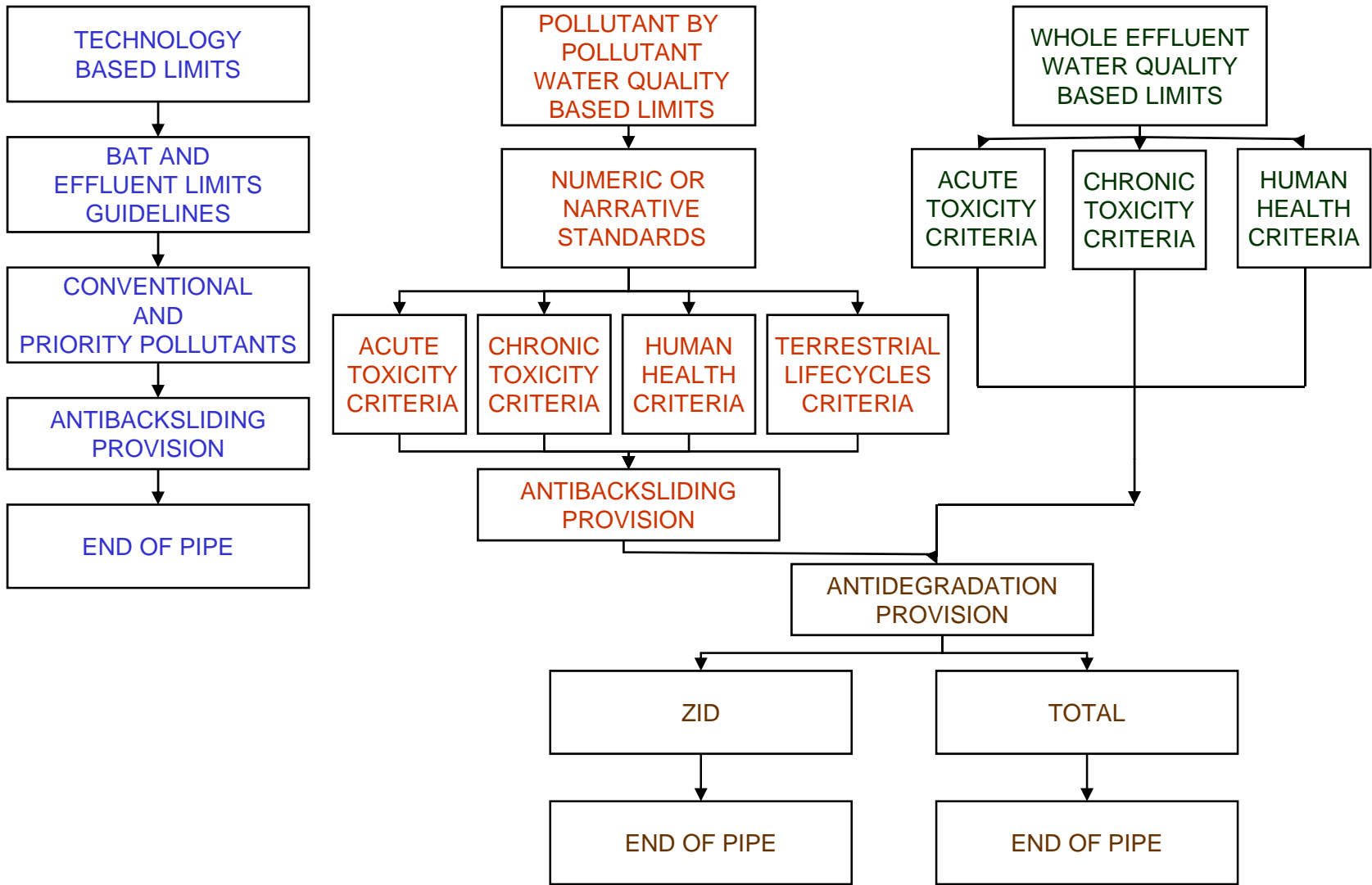


FIGURE 2
 CLEAN WATER ACT OF 1987
 WATER QUALITY-BASED TOXICS CONTROL

3. Purpose of Mixing Zones

- Achieve Maximum Dispersion in Smallest Area
- Minimize Effects on Receiving Water
- Minimize Acute and Chronic Toxicity in Receiving Stream
- Meet Narrative Water Quality Standards
- Provide Maximum Protection for Receiving Stream
- Maintain Zone of Passage for Fish
- Meet Local or National Mixing Zone Requirements
- Meet Technical Guidance

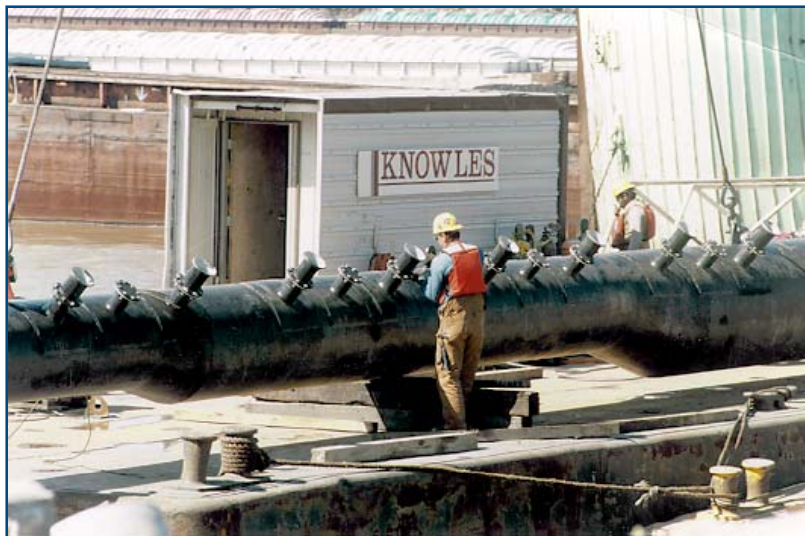
Oregon Guidelines for Mixing Zones

- Shall be free of concentrations that cause acute toxicity. The Department may on a case by case basis establish a zone of immediate dilution if appropriate for other parameters (including acute and chronic toxicity)
- Shall be free of Nuisance materials
- Limits shall be described in the wastewater discharge permit.
- Avoid overlap with other mixing zones
- Not threaten public health
- Minimize adverse effects on other designated beneficial uses outside the mixing zone

*From “Water Pollution; Division 41; ‘Statewide Water Quality Management Plan; Beneficial Uses, Policies, Standards and Treatment Criteria for Oregon”

Purpose of Diffusers

- Provide rapid and immediate dispersion of effluents to prevent adverse effects to the receiving stream



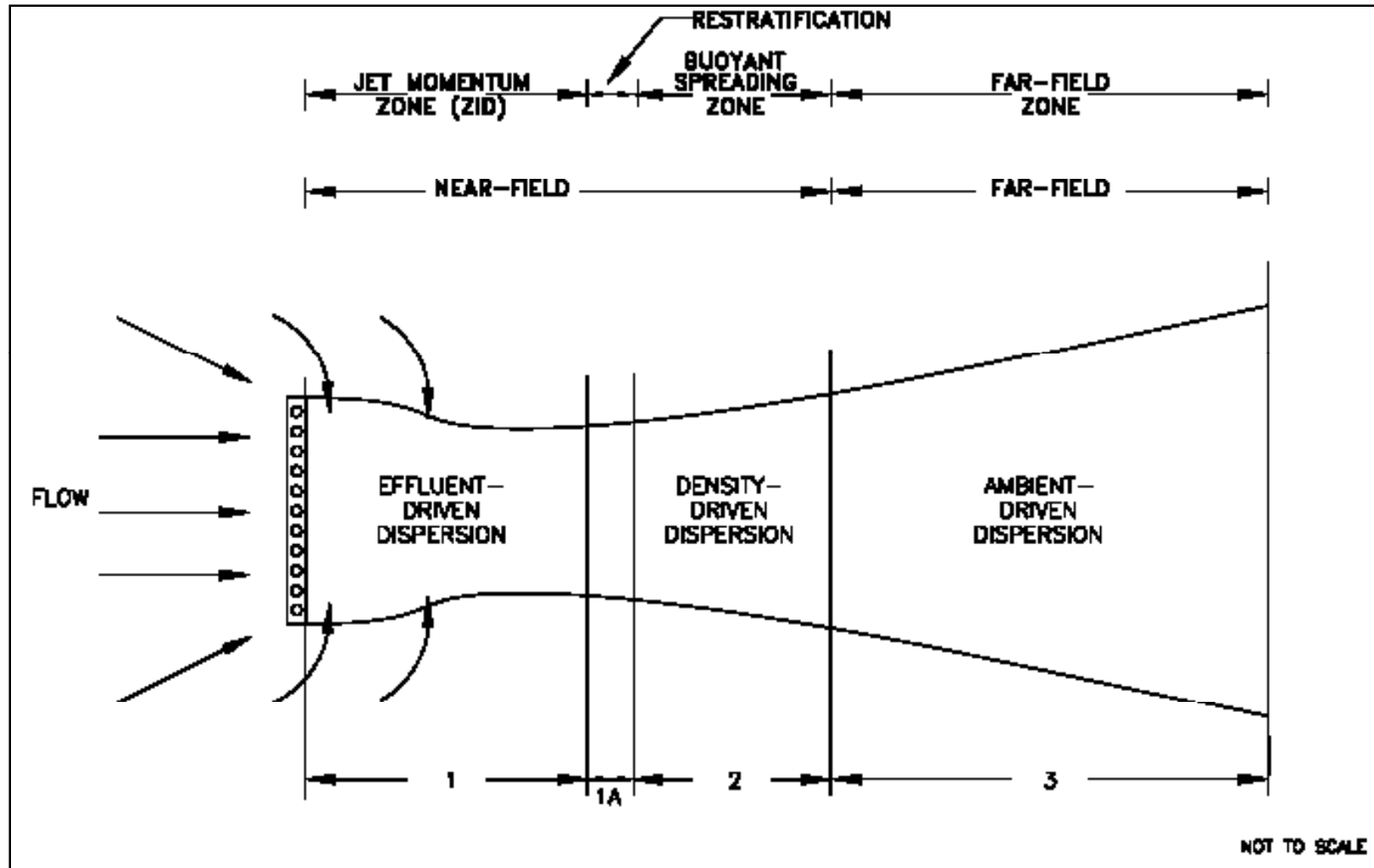


Diffusers

Purpose & Design Considerations

NEED RULES OF THUMB

5. Hydraulic Mixing Zone Concepts



- To Define the Dispersion from Effluent Momentum and Ambient Diffusion

Diffuser Design Considerations

- Effluent Mixing Zone
 - Zone of Initial Dilution (ZID)
 - Total Mixing Zone
- Enhancement of Mixing
 - Side Channel Discharge
 - Single-port or Multi-port Diffuser
 - Real-time Effluent Discharge (tidal or dynamic flows)
- Effluent River Influences on Mixing
 - River Hydraulics and Bathymetry
 - Effluent Flow and Discharge Velocity
 - Density Gradients
 - Flow Changes
 - Contaminant Build-up

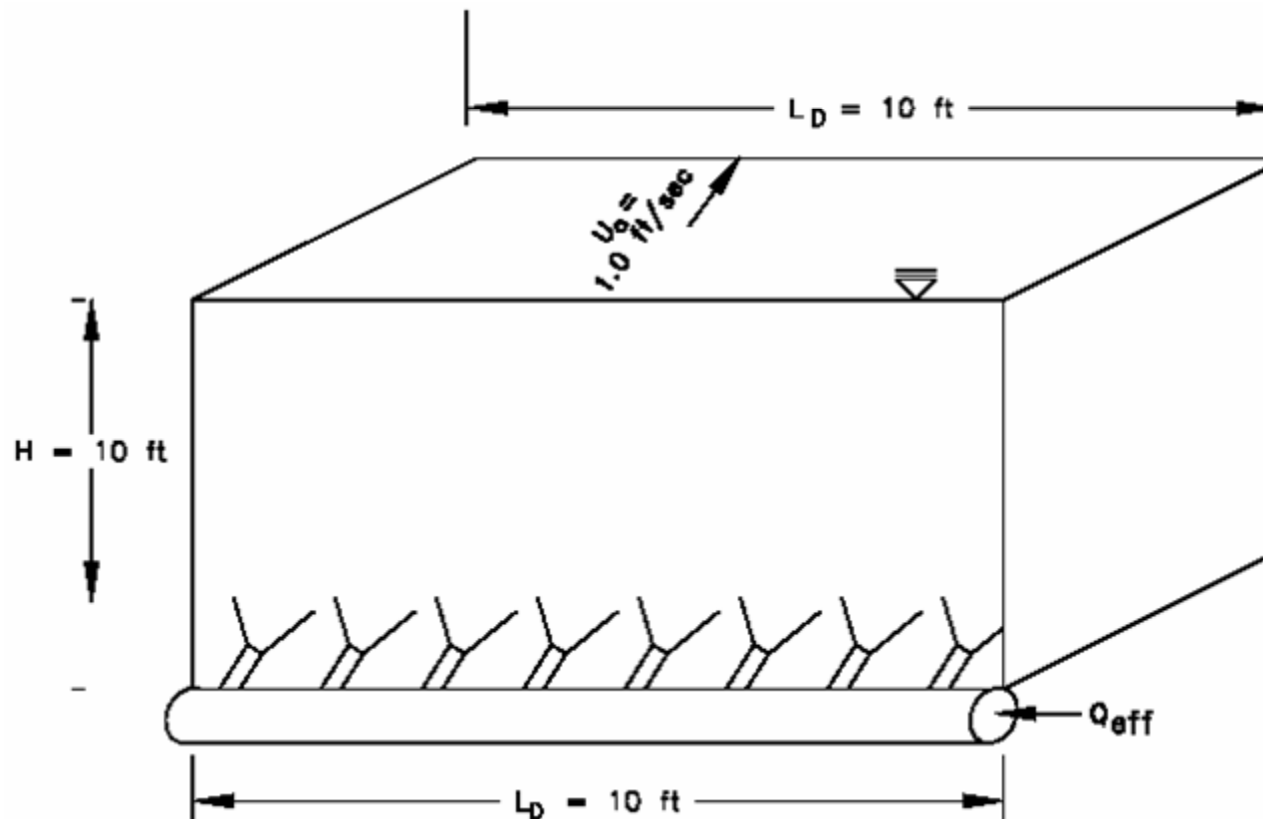
Zone of Initial Dilution (ZID) Cont'd

- Use EPA TSD Guidance
 - Use a high velocity diffuser ≥ 10 ft/sec to limit exposure to only a few minutes
 - Criterion Maximum Concentration (CMC) standards met:
 - 10% of distance from edge of outfall to edge of mixing zone in any spatial direction
 - Within 50 times the square root of the cross-sectional area of a single port in any spatial direction
 - Within distance of 5 times the local water depth in any spatial direction
 - Spatial is defined in the TSD as a discharge length scale or in the direction of flow. This is also mathematically defined along the centerline of the plume
- Hydraulically on the Order of 1 Diffuser Length (i.e., +/- 0.5 to 1.5 diffuser lengths, but dependent on ambient velocity). Cormix calculates the jet momentum zone to end at the 0.5 diffuser length

Total Mixing Zone (Chronic)

- TMZ is Far-field or Ambient Diffusion
- Far-field technically extends until effluent totally mixed with receiving stream – this may take 13 to 16 km or more
- No Chronic toxicity must be met at edge of this zone
- Zone of free passage limits TMZ in U.S. to 25% of cross-sectional area or volume of flow.

Bulk Dispersion Analysis

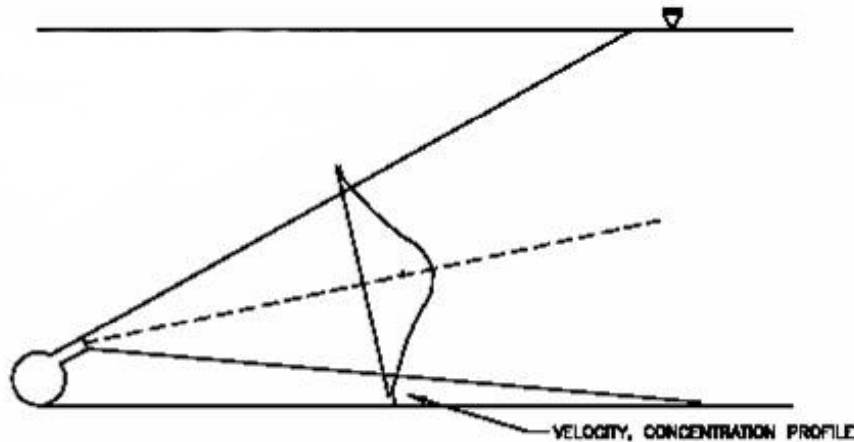


ESTIMATE OF DISPERSION = $\frac{(U_0 \cdot H \cdot L_D) + Q_{eff}}{Q_{eff}} = \frac{(1.0 \text{ ft/sec} \cdot 10 \text{ ft} \cdot 10 \text{ ft}) + 5 \text{ cfs}}{5 \text{ cfs}} = \frac{105 \text{ cfs}}{5 \text{ cfs}} = 21:1$

NOT TO SCALE

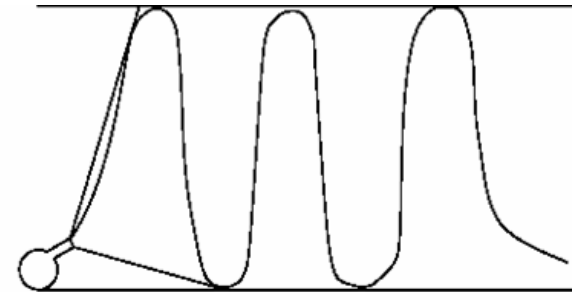
Plume Stability Analysis

STABLE (GAUSSIAN) PLUME



VELOCITY CONCENTRATION PROFILE

UNSTABLE PLUME



$$\frac{m_o}{p_o^{2/3} H} + \frac{m_a + m_o \cos \theta_o}{p_o^{2/3} H} \geq 0.54 \text{ unstable}$$

$$\frac{m_o}{p_o^{2/3} H} + \frac{m_a + m_o \cos \theta_o}{p_o^{2/3} H} < 0.54 \text{ stable}$$

Jirka (1982)

where:	m_o	= discharge momentum flux
	m_a	= ambient momentum flux
	p_o	= buoyancy flux
	H	= water depth
	q_o	= discharge angle

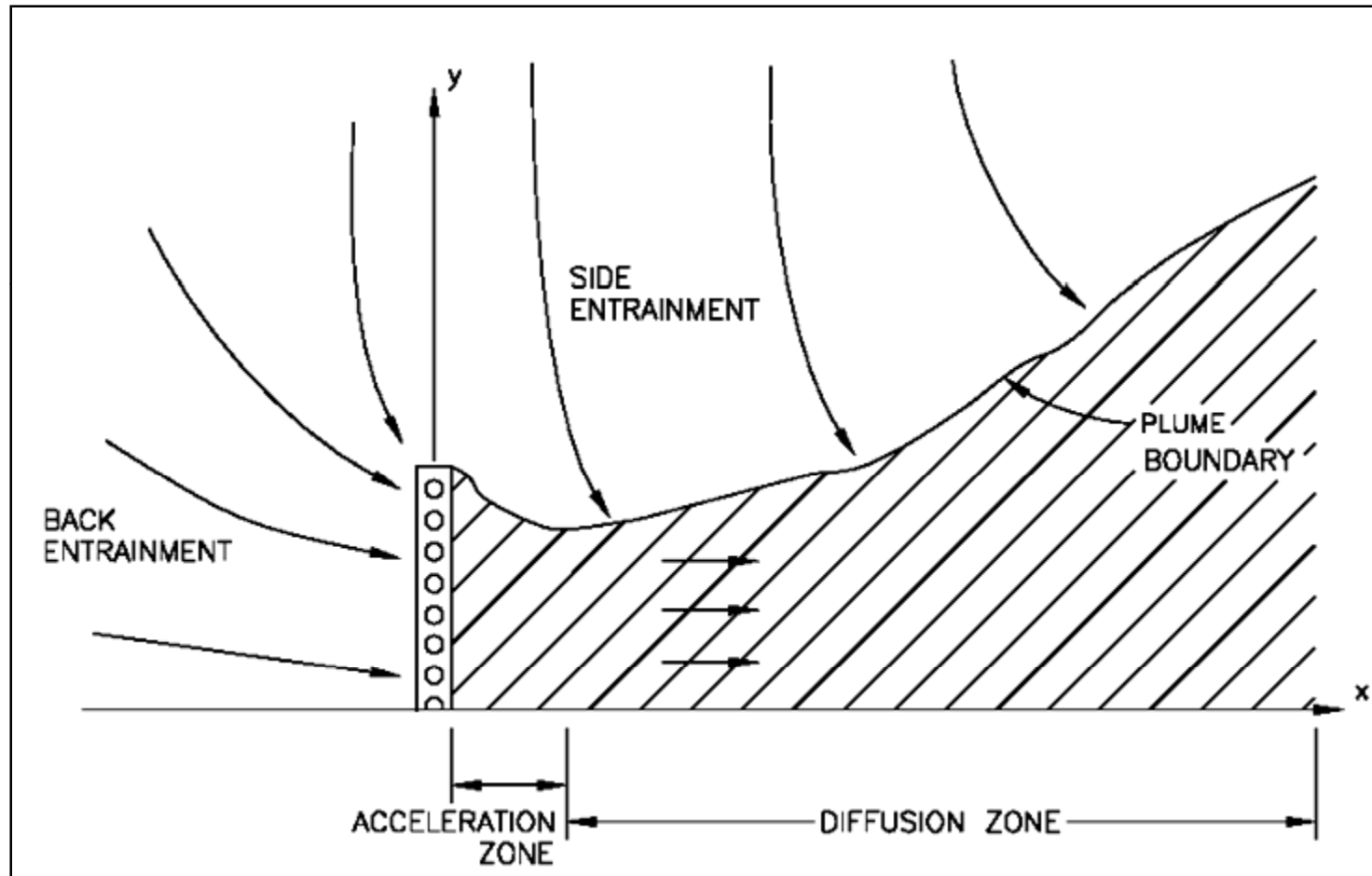
$$\frac{m_o (1 + m_o \cos^2 \theta_o)^2}{p_o^{2/3} H} + m_a \geq 0.54 \text{ unstable}$$

$$\frac{m_o (1 + m_o \cos^2 \theta_o)^2}{p_o^{2/3} H} + m_a < 0.54 \text{ stable}$$

Adams (1982), Jirka (1973,1982)

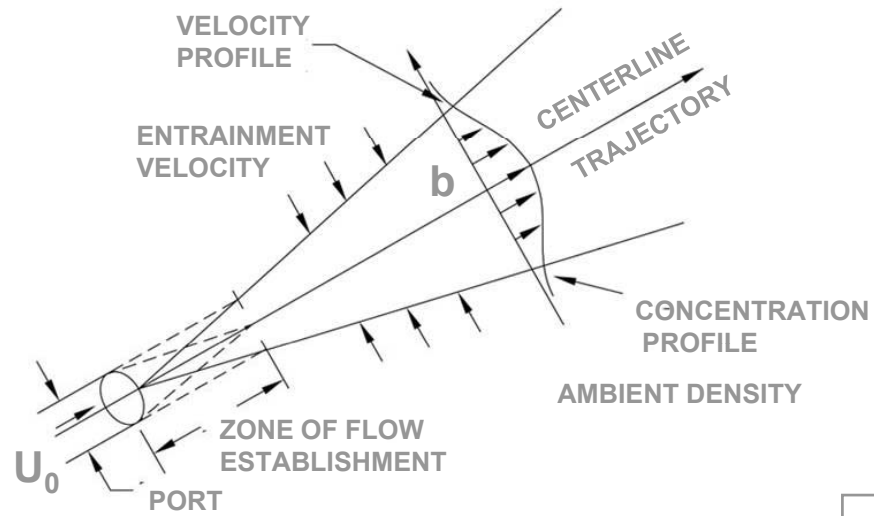
Jet Zone

Entrainment of Water (1/2 Plume)

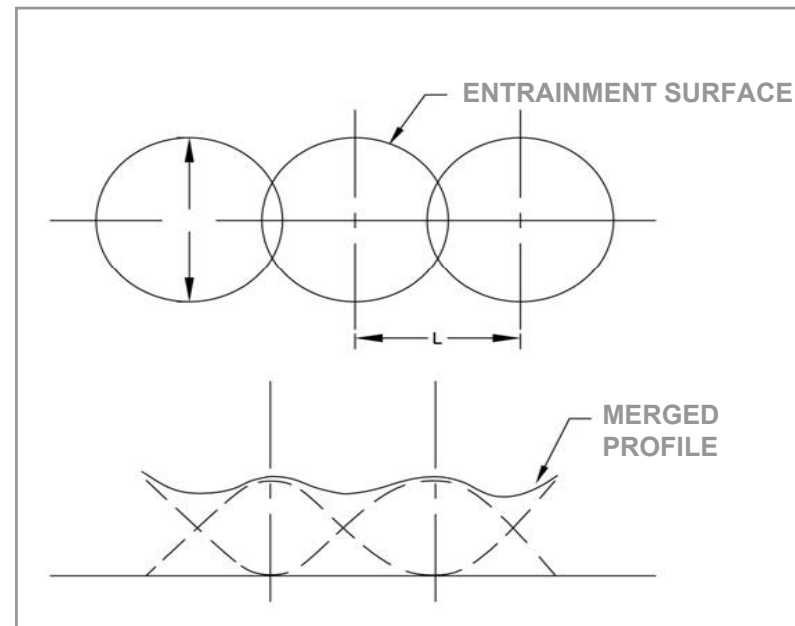


Stable Plume Analysis

(Plan View)



(Profile View)



UDKHDEN Dispersion Model Cont'd

o Zone of Flow Establishment

- Conservation of Mass: $\frac{d}{ds} \int_0^{\infty} Vrdr = E$
- Conservation of Energy: $\frac{d}{ds} \int_0^{\infty} V(T - T_{\infty})rdr = -\frac{dT_{\infty}}{ds} \int_0^{\infty} Vrdr$
- Conservation of Pollutant: $\frac{d}{ds} \int_0^{\infty} V(C - C_{\infty})rdr = -\frac{dC_{\infty}}{ds} \int_0^{\infty} Vrdr$
- Conservation of Momentum:

$$\frac{d}{ds} \int_0^{\infty} V^2 rdr = UE \sin(\theta_1) \cos(\theta_2) + \int_0^{\infty} \frac{g(\rho_{\infty} - \rho)}{\rho_d} rdr \sin(\theta_2)$$

o Zone of Established Flow:

$$POWER PROFILES = \left(1 - \left(\frac{r}{b} \right)^{\frac{3}{2}} \right)^2$$

for concentration, velocity, temperature, width,
and geometry to approximate Gaussian Profiles

o Zone of Merging

- Superimposition of Plume Property Distributions

UDKHDEN Dispersion Model Cont'd

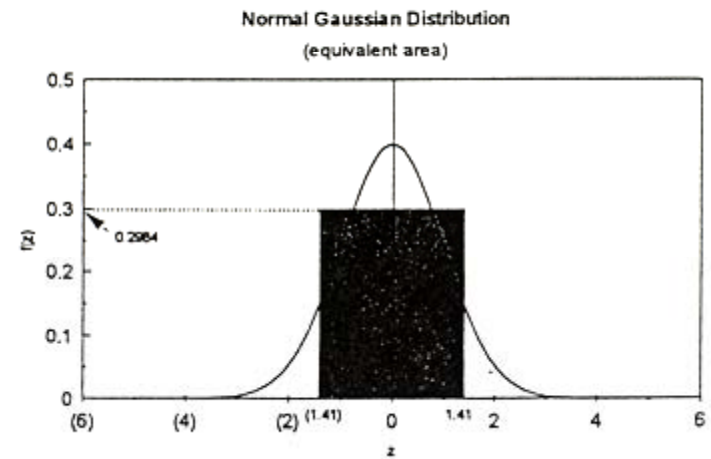
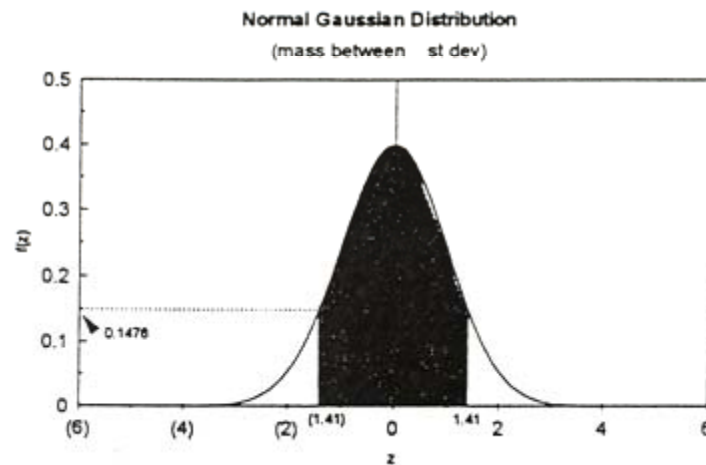
- Zone of Established Flow:

$$POWER\ PROFILES = \left(1 - \left(\frac{r}{b}\right)^{\frac{3}{2}}\right)^2$$

for concentration, velocity, temperature, width, and geometry to approximate Gaussian Profiles

- Zone of Merging
 - Superimposition of Plume Property Distributions

Equivalent Areas (“FAD”)



ZID-FAD = CENTERLINE DISPERSION / 0.7481 (+/- 1.41 SIGMA)

TMZ-FAD = CENTERLINE DISPERSION / 0.7909 (+/- 1.25 SIGMA)

Restratification

- o For Holley and Jirka (1986) restratification will occur if the densimetric Froude number is less than a critical value:

$$\frac{u_a}{\sqrt{|g'|}H} < 0.6 \text{ to } 0.7$$

where:	u_a	= ambient velocity (ft/sec)
	$ g' $	= buoyant acceleration (ft/sec ²)
		= $ g \Delta\rho/\rho_a $
	$\Delta\rho$	= residual density difference between ambient and effluent
		= $ \rho_a - \rho /S$
	ρ_a	= ambient density
	g	= acceleration due to gravity (ft/sec ²)
		= 32.2 ft/sec ²
	S	= dispersion at the end of the JMZ
	H	= water depth (ft)

Bouyant Spreading Zone Residual Plume Velocity

$$u_i = \frac{2S_i Q_e}{L_D H}$$

where:

- u_i = Plume velocity at the end of the jet momentum zone (ft/sec)
- S_i = Dispersion at the end of the jet momentum zone
- Q_e = Effluent flow in (ft³/sec)
- L_D = Diffuser length (ft)
- H = Local water depth (ft)

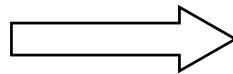
Plume velocity at the end of the Jet Momentum Zone (JMZ) during November field study:

$$S_i = 88:1 \text{ (66 divided by 0.7481)}$$

$$Q_e = 14 \text{ mgd}$$
$$= 21.7 \text{ ft}^3/\text{sec}$$

$$L_D = 100 \text{ ft}$$

$$H = 15 \text{ ft}$$



$$u_i = \frac{2(88)(21.7 \text{ ft}^3 / \text{sec})}{(100 \text{ ft})(15 \text{ ft})}$$
$$u_i = 2.55 \text{ ft} / \text{sec}$$

For comparison:

Ambient current velocity: 2.38 ft/sec

Port exit velocity: 8 ft/sec

End of Buoyant Spreading Regions Plume Velocity

$$u = u_i e^{-\phi(x-x_i)} \left[1 + \beta \left[1 - e^{-\phi(x-x_i)} \right] \right]^{-0.5}$$

where:

u = velocity at end of BSZ (ft/sec)

u_i = velocity at end of JMZ (ft/sec)

φ = $f_o / (8H)$

f_o = Moody friction factor = 0.035

H = local water depth (ft)

φ = $0.035 / [8 (15 \text{ ft})]$
= 0.000292 ft⁻¹

x = distance downstream from **x_i**

x_i = distance at end of JMZ (ft)

β = $2a_2 / (l_i b_i \phi)$

b = $[2(0.068)] / [(0.8862)(50 \text{ ft})(0.000292 \text{ ft}^{-1})]$
= 10.52

a₂ = entrainment coefficient = 0.068

l_i = $\sqrt{\pi}/2 = 0.8862$

b_i = $0.5 L_D = 50 \text{ ft}$

L_D = diffuser length (ft) = 100 ft

At the end of an intermediate zone: $b = b_i \left[e^{\phi(x-x_i)} (1 + \beta) - \beta \right]$

where: **b** = plume width at end of BSZ (ft)

b_i = plume width at end of JMZ (ft)

At the end of the BSZ: $S = S_i \left[1 + \beta \left(1 - e^{-\phi(x-x_i)} \right) \right]^{-0.5}$

where: **S** = dispersion at end of BSZ

S_i = dispersion at end of JMZ

Far-field Dispersion

$$c(x, y, z) = \frac{C_0 Q_0}{4(z_2 - z_1)u(\pi D_y x / u)^{0.5}} * \sum_{n=-\infty}^{n=+\infty} \sum_{m=-\infty}^{m=+\infty} F_1 * F_2$$

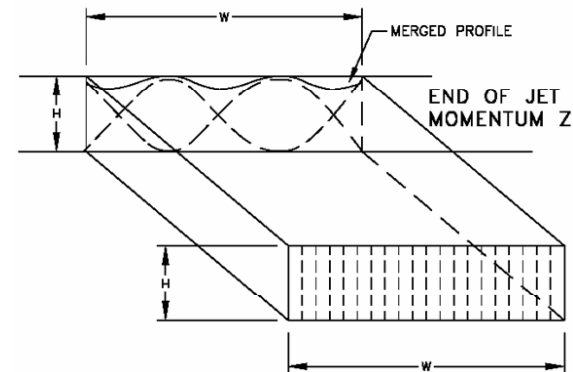
where:

$$F_1 = \exp\left[-\frac{(y - y_0 - 2nB)^2}{4D_y x / u}\right] + \exp\left[-\frac{(y + y_0 - 2nB)^2}{4D_y x / u}\right]$$

$$F_2 = \operatorname{erf}\left[\frac{z + z_2 - 2mH}{2(D_z x / u)^{0.5}}\right] - \operatorname{erf}\left[\frac{z + z_1 - 2mH}{2(D_z x / u)^{0.5}}\right] + \operatorname{erf}\left[\frac{z - z_1 - 2mH}{2(D_z x / u)^{0.5}}\right] - \operatorname{erf}\left[\frac{z - z_2 - 2mH}{2(D_z x / u)^{0.5}}\right]$$

and where:

$C(x,y,z)$	= concentration at location x,y,z (units)
x	= distance downstream from line source (ft)
y	= distance from channel bank (ft)
y_0	= location of line source from channel bank
z_1	= distance from water surface to top of line source (ft)
z_2	= distance from water surface to bottom of line source (ft)
u	= ambient river velocity
D_y	= lateral dispersion coefficient (ft ² /s)
	= bu^*/H
b	= 0.23 for long straight channels
u^*	= shear velocity (ft/sec)
	= $3.8 u n / (H)^{1/6}$
n	= Manning's n = 0.035
D_z	= vertical dispersion coefficient
	= $D_y/3$
H	= river depth (ft)
B	= river width (ft)
Q_0	= initial source flow (ft ³ /sec)
C_0	= initial source concentration (units)
erf	= error function
n, m	= indices



NOTE: PLANE SOURCE
MODELED AS INDIVIDUAL,
EQUAL, LINE SOURCES

Jet Momentum: Unstable Plume Analysis

(Shallow Water Diffusers)

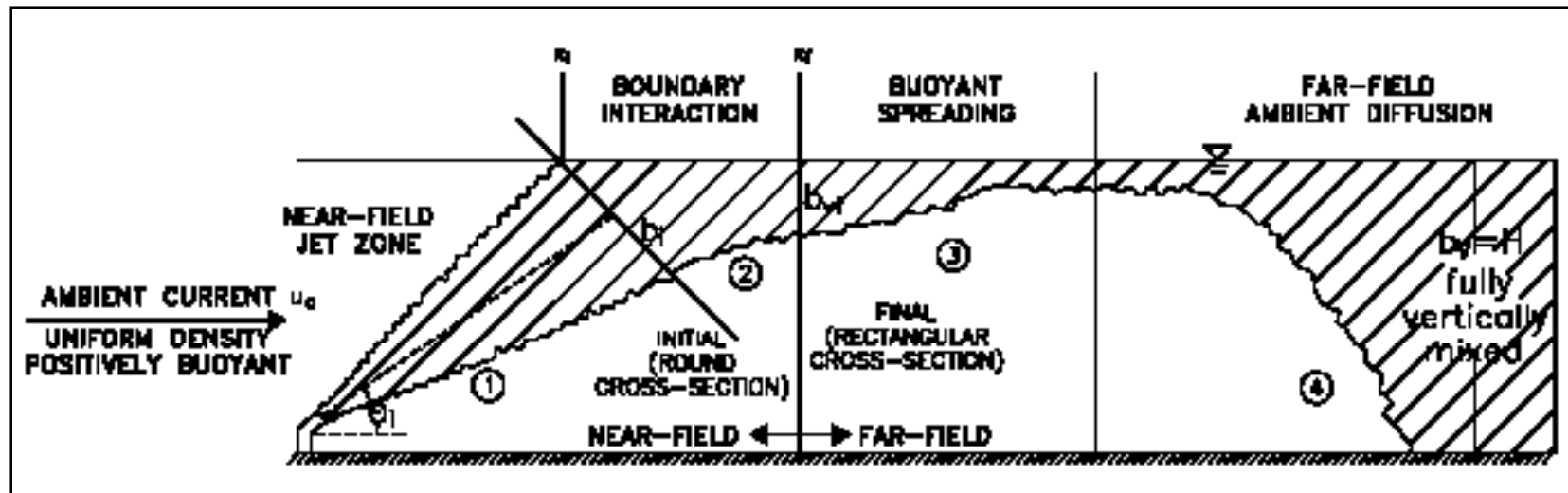
Holley and Jirka 1986

$$S = \frac{1}{2}V + \frac{1}{2} \left(V^2 + \frac{2m_o H}{q_o^2} \cos^2 \theta_o \right)^{0.5}$$

where:

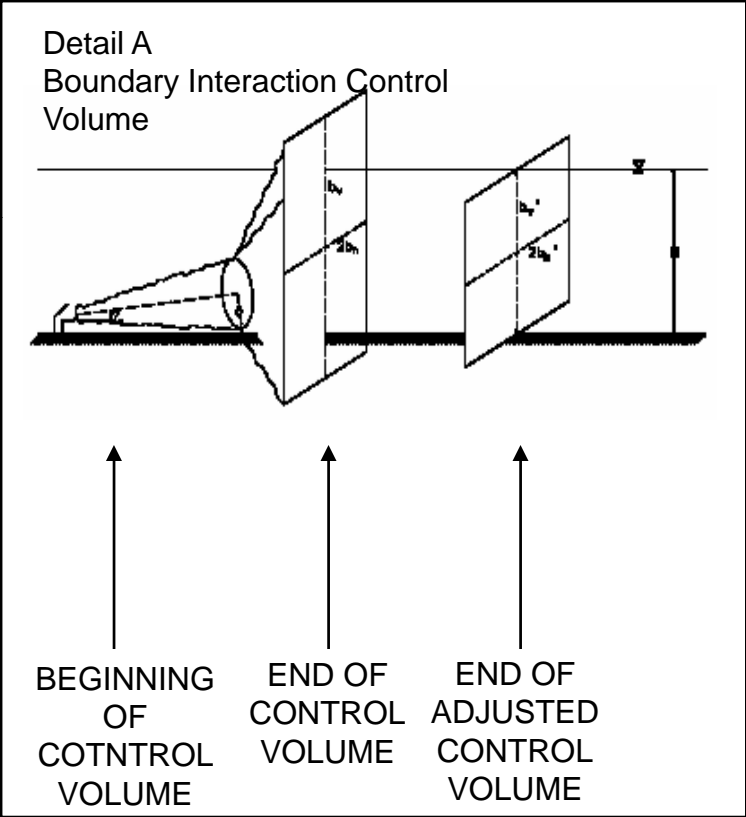
- S = bulk dispersion (___:1, dimensionless)
- V = volume flux ratio,
or ambient mixing due to ambient current
= $u_a H / q_o$
- H = water depth
- q_o = discharge flux per unit length
= $u_o a_o / L$
- m_o = momentum flux (ft³/sec²)
= $u_o^2 a_o / L$
- L = port spacing
- a_o = port area (ft²)
- u_o = port exit velocity
- θ_o = port discharge angle

CORMIX Schematic for Dispersion From a Diffuser

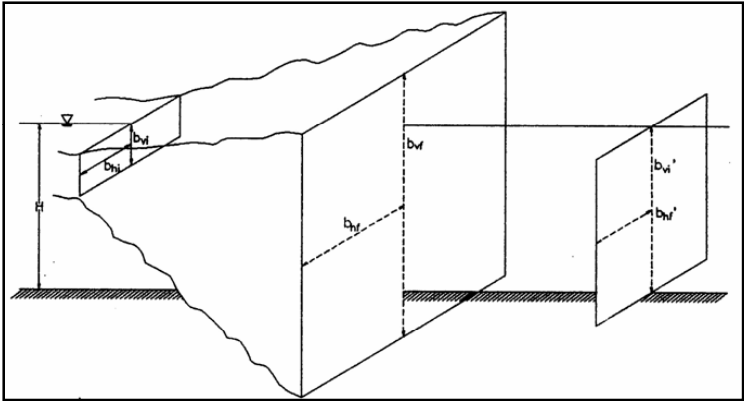


CORMIX Schematic

Near-field Dispersion



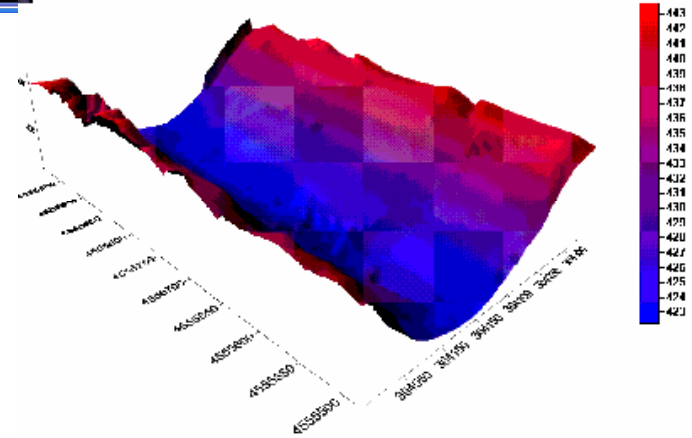
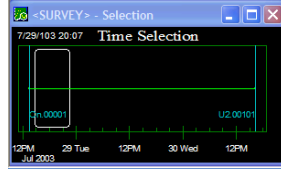
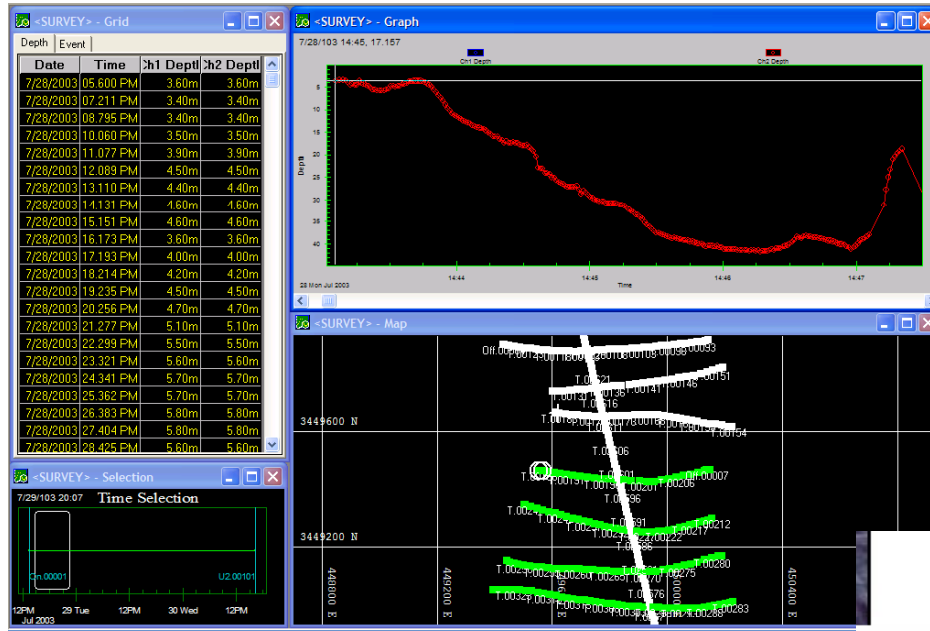
Far-field Dispersion



Data Required for Designing a Diffuser

- o Bathymetry
- o Effluent and Background Water Quality
- o River Stage and Velocity
- o Dye Monitoring

Bathymetry



Discharge/Velocity Measurements



Dye Dispersion



Pump Set Up



AquAeTer, Inc.

optimizing environmental resources – water, air, earth

Michael R. Corn, P.E.
AquAeTer, Inc.,
Brentwood, TN
(615) 373-8532
mcorn@aquaeter.com

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